or more, and a particle strength of 50 kg/cm^2 or more, under mixing conditions such that said (a) component does not substantially undergo breakdown, to give a mixture; wherein said base particle is obtained by spray-drying an aqueous slurry and

(II): mixing the mixture obtained in step (I) with 5 to 100 parts by weight of fine powder, based on 100 parts by weight of the mixture, with substantially maintaining the shape of (a) component containing (b) component, to give detergent particles,

Sub C1 cont'd

wherein the detergent particles have a degree of particle growth of 1.3 or less, and a bulk density of 500 g/L or more.

B1 cont'd

2. (Amended) The process according to claim 1, wherein in said step (I), a mixing operation is carried out by using a mixer comprising agitation impellers of which mixing impellers have a shape of a paddle, wherein the agitation impellers have a Froude number of from 0.5 to 8, provided where the mixer further comprises disintegration impellers, the mixing operation is carried out under mixing conditions so as not to substantially rotate the disintegration impellers.

3. (Amended) The process according to claim 1, wherein in said step (I), a mixing operation is carried out by using a mixer comprising agitation impellers of which mixing impellers have a shape of a screw, under mixing conditions wherein the agitation impellers have a Froude number of from 0.1 to 4.

Sub C2

B1 cont'd

Sub C2 cont'd

4. (Amended) The process according to claim 1, wherein in said step (I), a mixing operation is carried out by using a mixer comprising agitation impellers of which mixing impellers have a shape of a ribbon, under mixing conditions wherein the agitation impellers have a Froude number of from 0.05 to 4.

B2

13. (Twice Amended) The process according to claim 1, wherein the detergent particles have a dissolution rate of 90% or more, under conditions where the resulting detergent particles are supplied in water at 5°C; stirred for 60 seconds under the stirring conditions that 1 g of the detergent particles are supplied to a one-liter beaker having an inner diameter of 105 mm which is charged with one-liter of hard water having 71.2 mg $CaCO_3$/L, wherein a molar ratio of Ca/Mg is 7/3, and stirred with a stirring bar of 35 mm in length and 8 mm in diameter at a rotational speed of 800 rpm; and filtered with a standard sieve having a sieve-opening of 74 μm as defined by JIS Z 8801, wherein the dissolution rate of the detergent particles is calculated by the equation:

Dissolution Rate (%) = [1 - (T/S)] × 100

wherein S is a weight (g) of the detergent particles supplied; and T is a dry weight (g) of insoluble remnants of the detergent particles remaining on the sieve when an aqueous solution prepared under the above stirring conditions is filtered with the sieve, B2 cont'd

wherein drying conditions for the insoluble remnants are kept at a temperature of 105°C for 1 hour, and then in a desiccator with a silica gel at 25°C for 30 minutes.